

### Properties of Silicon Melt

$$\frac{1}{6} \cdot \text{Hz} = 10 \cdot \frac{1}{\text{min}} = \text{rpm}$$

$$\omega := 2 \cdot \pi \cdot \frac{1}{6} \cdot \text{Hz}$$

$$D_{\text{boule}} := 30 \cdot \text{cm}$$

$$R_g := 1.98 \cdot \frac{\text{cal}}{\text{mole} \cdot \text{K}}$$

$$\text{nm} := 10^{-9} \cdot \text{m}$$

$$\mu\text{m} := 10^{-6} \cdot \text{m}$$

$$\rho := 2.33 \cdot \frac{\text{gm}}{\text{cm}^3}$$

$$\nu := \frac{\mu}{\rho}$$

$$D := 8 \cdot 10^{-4} \cdot \frac{\text{cm}^2}{\text{s}}$$

$$\mu := 0.1 \cdot \text{poise}$$

$$M_w := 28 \cdot \frac{\text{gm}}{\text{mole}}$$

$$\nu = 4.292 \times 10^{-6} \cdot \frac{\text{m}^2}{\text{s}}$$

$$\Delta H_f := 50550 \cdot \frac{\text{joule}}{\text{mole}}$$

$$C_p := 0.71 \cdot \frac{\text{joule}}{\text{gm} \cdot \text{K}}$$

$$k := 1.48 \cdot \frac{\text{watt}}{\text{cm} \cdot \text{K}}$$

$$T_{\text{eq}} := 1685 \cdot \text{K}$$

$$S(T) := \exp\left(\frac{-\Delta H_f}{R_g} \cdot \frac{T - T_{\text{eq}}}{T}\right)$$

$$C_{\text{eq}} := \frac{\rho}{M_w}$$

$$\alpha := \frac{k}{\rho \cdot C_p}$$

$$\text{Flux}_C(S) := 0.62 \cdot D^{\frac{2}{3}} \cdot C_{\text{eq}}^{-\frac{1}{3}} \cdot \nu^{-\frac{1}{6}} \cdot \omega^{\frac{1}{2}} \cdot (S - 1)$$

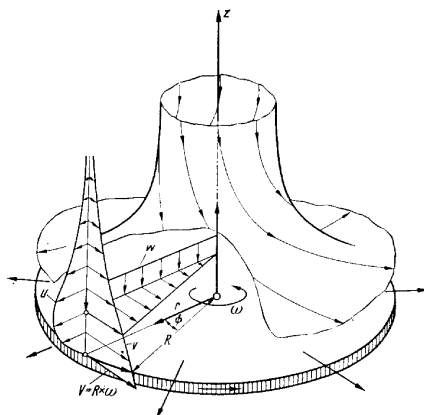
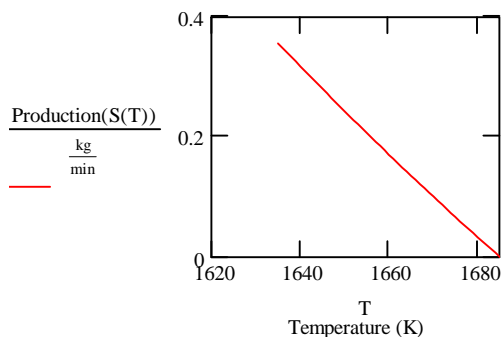
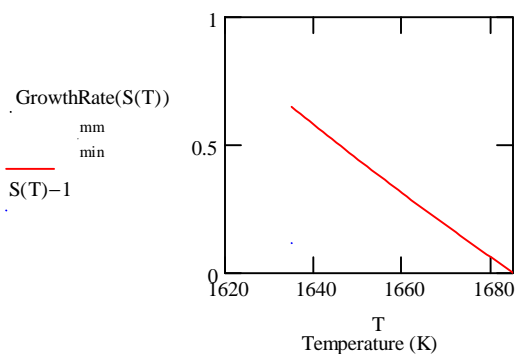
$$\text{Flux}_C(S(T_{\text{eq}} - 30 \cdot \text{K})) = 0.521 \cdot \frac{\text{mol}}{\text{m}^2 \cdot \text{s}}$$

$$\text{GrowthRate}(S) := \frac{\text{Flux}_C(S) \cdot M_w}{\rho}$$

$$T := T_{\text{eq}} - 50 \cdot \text{K} \dots T_{\text{eq}}$$

$$\text{Production}(S) := \text{GrowthRate}(S) \cdot \frac{\pi}{4} \cdot D_{\text{boule}} \cdot \rho$$

### Growth of Silicon Boule limited by BL-Mass Transfer



**Mass Transfer Heat Transfer Analogy**

$$Sh(r) := \left( 0.62 \cdot r \cdot D^{-1/2} \cdot \nu^{-1/4} \cdot \omega^{1/4} \right)^2$$

$$Sc := \frac{\nu}{D}$$

$$Re(r) := \frac{(r \cdot \omega) \cdot r}{\nu}$$

$$Sc = 53.648$$

$$Re(10\text{-cm}) = 2.44 \times 10^3$$

$$h := Nu(r) \cdot \frac{k}{r} \quad Pr := \frac{\nu}{\alpha}$$

$$Pr = 0.048$$

$$j_M(r) := \frac{Sh(r)}{Re(r) \cdot Sc} \cdot Sc^2$$

$$f(r) := 2 \cdot 0.62 \cdot Re(r)^{-1/2}$$

$$j_H(r) := \frac{Nu(r)}{Re(r) \cdot Pr} \cdot Pr^2$$

$$j_H = j_M = \frac{f}{2}$$

$$Sh(r) := 0.62 \cdot Re(r)^{1/2} \cdot Sc^{1/3}$$

$$Nu(r) := 0.62 \cdot Re(r)^{1/2} \cdot Pr^{1/3}$$

**Nu was Derived from MT HT Analogy above**

$$h := 0.62 \cdot \left[ \left( \frac{\omega}{\nu} \right)^{1/2} \cdot Pr^{1/3} \right] \cdot k$$

$$Flux_H(T) := \frac{h \cdot (T_{eq} - T)}{\Delta H_f} \quad Flux_H(T_{eq} - 30 \cdot K) = 9.774 \frac{\text{mol}}{\text{m}^2 \cdot \text{s}}$$

$$GrowthRate_H(T) := \frac{Flux_H(T) \cdot M_w}{\rho}$$

$$Production_H(T) := GrowthRate_H(T) \cdot \frac{\pi}{4} \cdot D_{boule} \cdot \rho$$

**Growth of Silicon Boule limited by BL-Heat Transfer**

